INTRODUCTION

Soap is an important surface-active agent and it is chemically the alkali metal salts of long-chain fatty acid. The most commonly used fat and oils for production of soap through saponification reactions are animal fallow, coconut oil, and palm oil, palm kernel oil and linoseed oil. Similarly, potassium and sodium hydroxide are widely used as caustic alkalis for the purpose. The demand for these materials for various other domestic and industrial application are high resulting in their high costs. Consequently, there is a need to explore unconventional sources of oils and caustic alkalis for the production of soap and to determine by means of kinetic approach, the optimum reacting conditions for efficiency and utilization of the process. Several workers reported the use of caustic alkalis from ash for soap production and the effects of a number of factors, notably temperature, ash particle size, etc on the yield of caustic alkali.

The physico-chemical characteristics of seed oils from plant in the world have been reported. One of such oil is obtained from a Treculia africana and has saponification value of 1960. It is found mainly in the south east and south-south zone in the country. The percentage of seed oil is significant. The seed is a rich source of protein, carbohydrate, vitamins and also a possible source of raw materials for the production of vegetable oils, soaps etc.

This present study is aimed at determining the appropriate reacting conditions that will improve the viability of the saponification process of locally sourced alkali with an unconventional source of oil via kinetic studies. It will also establish a suitable alternative to the usual palm kernel oil or in special case, coconut oil for use for quality toilet soap production, using raw materials which are locally obtained in Nigeria.

MATERIAL AND METHODS

The breadfruit seed used was obtained from a local market in Onitsha, pulverized with a grinding machine. A measured amount of the
pulverized cake was introduced into a thimble and the solvent (n-hexane) 100m/s was poured into the extractor flash and heat was applied. It was allowed for over 20-25 minutes for complete extraction of the oil. The procedure was repeated severally to obtain much quantity of the oil. The miscella was then distilled in an oven at 105°C for 2 hours to recover the solvent and to concentrate the oil via distillation process.  

The alkali use in this study was obtained by dissolving 120g of sieved ash of burnt female palm bunch in a distilled water agitated for 5 minutes and allowed to stand for 12 hours. The material was decanted and the brownish filtrate was heated. The temperature was maintained at 40°C for 10 minutes. The bleached alkali was separated from the spent earth by filtration using whatman A1 (24cm) filter paper on conical flask to recover the alkali (KOH) which was then water-clear. The concentration of the solution of local alkali (ngu) produced was determined after bleaching the ngu extract with active earth to water-clear. It was further concentrated by boiling and evaporation for some hours. 5mls of the solution of NGU extract was titrated against freshly made 0.5m HCL for the kinetic study, three different concentrations of the alkali extract was used (1.59mol/L, 2.58Mol/L and 5.08 mol/L).  

The fully boiled process of soap production was used in the saponification of *traculie African* oil using local alkaline extract. 50ml of the oil was measured into a beaker and a steam generator was introduced to raise the temperature to about 710°C (This exposes the free fatty acids present in the oil). After 2 minutes of heating, the oil was left to cool at 40°C.  

5g of the oil dissolved in 20ml of the fat solvent (ethanol) was introduced into a beaker containing 20ml of 5.08mol/L of the KOH (Ngu) and the mixture was constantly stirred. An aliquot, 5ml of the broth was taken every 3 minutes into a conical flask that contain 20ml of 10°C old distilled water and shaken. The content was then titrated against 0.5M HCL to a phenolphthalein end point and the litre values recorded. The experiment was repeated for different concentration of the KOH (Ngu); 2.58mol/L and 1.59/Mol/L respectively.  

5ml of the saponifying mixture was withdrawn at interval of 3 minutes and titrated against 0.5MHCL as above to determine the residual concentration of the KOH in NGU, until the concentration reduced to a constant value when the saponification was complete.  

With these values appropriate plots were produced (KOH/KOH) against time to obtain both the order of reaction, reaction constant K to confirm the result, the half life plot was also produced.  

**RESULTS AND DISCUSSION**  

In the reaction between the *traculie Africana* (Bread fruit) oil and NGU (KOH) a local alkali extract, the dominant fatty acid contained in the oil are linoleic and oleic acids. These fatty acids were hydrolysed according to the following steps.

**Splitting the oil**

\[
(18H31COO)_3 C_3H_5 + 3H_2O \rightarrow (18H31COOH + C_3H_5COH)_3
\]

The above equation refers to the splitting of the oil into fatty acid and glycerol

**The Neutralizing step**

\[
(18H31COO) + KOH + \rightarrow (18H31COOK + H_2O
\]

the rate equation is thus

\[
r_{KOH}=\frac{d(KOH)}{dt} = K (K_{OH})
\]

\[
\frac{dC_{KOH}}{C_{KOH}} = kdt
\]

Integrating with respect to times at limit 0 – t

\[
\frac{-dC_{KOH}}{C_{KOH}} = kdt
\]

Then the plates of ln (CkoH/CkoHt) versus time (t), produced straight line (Fig.1-4). This shows that the reaction between the breadfruit oil are NGU (KOH) was essentially first order and the rate constant (kc) averaged to 0.0696min⁻¹. calculating the half life based on the concentration (K_{ono}=2.58mol/L) as in figure II, the result obtained...
Fig. 1: \( \ln(C_{\text{KOH},0}/C_{\text{KOH},t}) \) versus time, \( t \), for \( C_{\text{KOH},0} = 5.08 \) moles/l in the saponification of breadfruit oil

\[ y = 0.07844x + 1.2405 \]

Fig. 2: \( \ln(C_{\text{KOH},0}/C_{\text{KOH},t}) \) versus time, \( t \), for \( C_{\text{KOH},0} = 2.58 \) moles/l in the saponification of breadfruit oil

\[ y = 0.00344x + 0.3155 \]
Fig. 3: $\ln\left(\frac{C_{KOH,0}}{C_{KOH,t}}\right)$ versus time, $t$, for $C_{KOH,0} = 1.59$ moles/l in the saponification of breadfruit oil

Fig. 4: half-life curve at $C_{KOH,0} = 2.58$ moles/l
confirmed a typical first order reaction with $t_{1/2} = 9.96$ minutes.8.

The reaction (saponification process) was observed to increase with initial concentration of the Ngu. This was why the saponification of breadfruit oil with Ngu (KOH) was concentration and time dependent. Nevertheless, a high quality soap was produced in the process7,9.

Figure 4 show, the effect of changes in concentration of KOH with time at various initial concentration of KOH. When $C_{koh0} = 5.08$ml/l, the saponification reaction between breadfruit and KOH (Ngu), came to completion at a faster rate and it took the total alkali 23 minutes to be consumed in the reaction10. On the other hand, as the relative initial concentrations were reduced by serially diluting the KOH, with distilled water, to obtain lesser concentration of $KOH_0 = 2.58$ml/L and $C_{koh0} = r.59$mol/L respectively. The duration of the reaction was progressively becoming slower with time limit extending to 33 and 39 minutes respectively. This phenomenon indicates that the reaction is evidently concentration dependent8.

When a graph of $\ln(C_{koh}/C_{koh0})$ was plotted against time for each of the concentrations, the curves obtained (figure I-III) were straight lines with positive magnitude. The calculated concentrations at instant for the reactions $\ln(C_{koh}/C_{koh0})$, while the curves for the order of reaction and reaction constant are shown in figure I-II, the half life curve was produced in Fig. 4.10.

CONCLUSION

A first order reaction was obtained in the saponification of breadfruit oil with Ngu. The average rate constant was 0.069 min $^{-1}$. and the half life value of 9.96 minutes, the reaction rate was a function of the initial concentration of local alkali. The soft soap produced could be modified into a hard soap. Notwithstanding the overall cost of production of a high quality, long lasting and wonderful lather soap using these raw materials makes it economically attractive. The results of this work is reliable for use in the design of a hydrolyser for commercial processing.

REFERENCES

